

Monolayer dispersion of oxides and salts on surface of ZrO_2 and its application in preparation of ZrO_2 -supported catalysts with high surface areas

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The thermostability of ZrO_2 can be improved by dispersing a layer of an active component onto its surface in advance. The research results of seven kinds of catalysts (ZrO_2 -supported MoO_3 , WO_3 , CuO , SO_4^{2-} , NiO , FeSO_4 and Fe_2O_3) show that the surface areas of the samples prepared by impregnating $\text{Zr}(\text{OH})_4$ with the active components and then calcining at high temperature are much larger than those of the samples prepared with an ordinary method, namely, impregnating ZrO_2 calcined at high temperature. The surface areas of the ZrO_2 -supported catalysts obtained in this way are several times that of pure ZrO_2 calcined at the same temperature. The characteristic results show: (1) the active components are dispersed on the surface of ZrO_2 as monolayer; (2) there is a good corresponding relationship between the surface coverage and the surface area of the sample; (3) as the loading of an active component comes up to its utmost dispersion capacity, the surface area of the sample will be the largest. The mechanism responsible for these phenomena has been discussed.

Keywords: monolayer dispersion, ZrO_2 -supported catalysts, highly specific surface

1. Introduction

An ordinary method of preparing oxide-supported catalysts is that the support is calcined in order to turn the hydrous oxide into the oxide and stabilize its texture, then it is impregnated with the solution of an active component and calcined again. The pre-calcination temperature of the support is often equal to or higher than the one at which the resulting catalyst is treated. For some classical supports such as $\gamma\text{-Al}_2\text{O}_3$ and silica gel, using this method one can easily obtain supported catalysts with high surface areas ($150\text{--}300\text{ m}^2/\text{g}$). Recently, zirconia as support is attracting considerable interest [1]. However, it is very difficult to obtain ZrO_2 -supported catalysts with high surface areas, because its original surface area is not very large and decreases rapidly during calcination at high temperature. Thus, its applications are thereby limited.

Recently, it has been realized that crystallite growth, accompanying phase transformation and inter-crystallite sintering should be responsible for degeneration of the texture of a support during calcination, and these processes occur via a mechanism of surface diffusion [1]. Several years ago, our research group proved that many oxides and salts can disperse onto surfaces of supports as a monolayer [2–4]. So we image that if a layer of active component is dispersed on the surface of a support to segregate the particles of the support from each other

before the particles have grown into bigger ones, its surface diffusion would be suppressed, and the thermostability of its texture would be improved, and as a result, a catalyst with high surface area would be obtained.

We reported that a $\text{MoO}_3/\text{TiO}_2$ catalyst with high surface area was obtained by adding a solution of $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}$ to $\text{Ti}(\text{OH})_4$ and then calcining it at 500°C for 4 h [5]. For example, the surface area of the catalyst with 13 wt% MoO_3 is $133\text{ m}^2/\text{g}$. However, the surface area of $\text{MoO}_3/\text{TiO}_2$ (with same MoO_3 content) obtained by impregnating TiO_2 crystallized at 500°C and then calcining at the same temperature is only $66\text{ m}^2/\text{g}$. We were also attentive to other authors' works and found some data that can be used to support our ideal. For example, Arata and Hino [6,7] prepared many new solid superacids by impregnating $\text{Zr}(\text{OH})_4$ with aqueous $(\text{NH}_4)_6(\text{H}_2\text{W}_{12}\text{O}_{40})$, $(\text{NH}_4)_2\text{SO}_4$ or $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}$, followed by evaporating the water, drying and then calcining at high temperature. From the papers they published we noticed that the surface areas of these superacids were much larger than that of pure ZrO_2 treated at the same temperature. In addition, Cimino et al. reported that CrO_3 addition can display a protective effect on the surface areas of specimens based on ZrO_2 only dried at 110°C [8].

In recent years, the method of doping of some oxides (surface doping or bulk doping) was used in studies on superplastic ZrO_2 ceramics [9] and SnO_2 gas-sensitive materials [10–12] to improve their thermostability and

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microstructure, and some inspiring results were obtained.

These facts indicate that the surface areas of the samples obtained by impregnating hydrous zirconia and then calcining are often larger than those of the samples obtained by impregnating the crystalline oxide. However, to date there have not been published systematic and detailed reports about it in the catalytic literature. Therefore, it is important to prove the generality of this phenomenon, to explore its origin and rule, and to make use of it to prepare some catalysts with high surface areas. In this paper, we will report the research results on several ZrO₂-supported catalyst systems that are valuable in application.

2. Experimental

2.1. Sample preparation

A solution of ammonia (3.3 M) was added dropwise into a solution of zirconyl chloride (1 M) under stirring until pH = 10. The precipitate was aged in the mother liquor for 24 h, then filtered and washed repeatedly with distilled water until a negative test for chloride ions was obtained. The chloride-free hydrogel was dried in air at 110°C for 24 h, then ground to proper particle size.

MoO₃/ZrO₂, WO₃/ZrO₂, CuO/ZrO₂, SO₄²⁻/ZrO₂, Fe₂O₃/ZrO₂, NiO/ZrO₂ and FeSO₄/ZrO₂ were prepared by impregnating the dried hydrogel with solutions of ammonium heptamolybdate, ammonium metatungstate, copper nitrate, ammonium sulfate, iron nitrate, nickel nitrate and iron sulfate respectively, then drying and calcining at designated temperature for 4 h.

For comparison, a portion of Zr(OH)₄ was calcined at 450–800°C for 4 h to turn it into ZrO₂, and some catalysts were prepared by impregnating the obtained ZrO₂. Zr(OH)₄ samples used in different catalyst systems were made in separate batches, therefore their specific surfaces are slightly different.

2.2. Sample characterization

X-ray diffraction. The identification of phases was carried out by means of a BD-86 X-ray diffractometer, employing Cu Kα (Ni-filtered) radiation.

Surface area measurement. The surface areas (SA) of all samples were measured using the BET method by N₂ adsorption at 77 K. Resultant surface areas were normalized to the values per gram support in order to compare with each other.

Raman spectra determination. Raman spectra were obtained with a Jobin-Yvon U-1000 monochromator. The 514.5 nm line of a Spectra-Physics model Stablite-2016 Ar⁺ laser was used for excitation. A laser power of 100 mW and the spectral slit width of 1 cm⁻¹ were applied.

XPS measurement. XPS spectra were obtained with a VG-ESCALAB5 spectrometer. As anode, Al Kα was employed, usually at 10 kV, 40 mA. The specimen was treated at 10⁻⁸ Torr. The energy of analysis chamber was fixed at 50 eV. The XPS peak intensity ratio between an appointed energy level of some element in an active component and Zr 3d was taken as a measurement of the surface concentration of the active component on ZrO₂.

DTA determination. DTA measurements were performed by a Dupont model 1090 apparatus, using α-Al₂O₃ as reference and a temperature rise rate of 20 K/min.

3. Results

3.1. MoO₃/ZrO₂ systems

3.1.1. BET surface areas

The SA of pure ZrO₂ obtained by calcining Zr(OH)₄ at 550°C for 4 h is 52 m²/g. After supporting MoO₃, its SA would decrease gradually with a rise in MoO₃ content.

The relationships between SA of the samples obtained by impregnating Zr(OH)₄ (dried at 110°C) with (NH₄)₆Mo₇O₂₄ solution and then calcining at 450, 550, 600, and 750°C respectively and their MoO₃ loadings are shown in table 1. The following facts are worthy of special mention:

(a) The surface areas of these samples are several times larger than that of the pure ZrO₂ calcined at the same temperature. This phenomenon is shown clearly for the samples calcined at higher temperature. For example, the SA of MoO₃/ZrO₂ with 0.16 g MoO₃/g ZrO₂ prepared by impregnating Zr(OH)₄ and then calcining it at 750°C is 101 m²/g ZrO₂, which is ten times that of ZrO₂ obtained by calcining pure Zr(OH)₄ at the same temperature.

(b) With the MoO₃ contents increasing, the surface areas of these samples calcined at a certain temperature increase and reach a maximum value (*S*_{max}), then decrease. The MoO₃ content corresponding to *S*_{max} depends on the calcination temperature of the sample.

Table 1
The surface areas of MoO₃/ZrO₂

MoO ₃ content (g/g ZrO ₂)	SA (m ² /g ZrO ₂)			
	450°C	550°C	600°C	750°C
0	96	52	32	10
0.03	131	87	60	52
0.09	156	140	84	96
0.16	218	186	135	101
0.26	307	224	189	97
0.31	310	210	175	–
0.42	304	159	143	78
0.51	255	104	120	47

At a lower calcination temperature, S_{max} is larger and the correspondent MoO_3 content is higher.

(c) For $\text{MoO}_3/\text{ZrO}_2$, the decline of SA with a rise in calcination temperature is much slower than for pure ZrO_2 . For example, as the calcination temperature rises from 450 to 750°C, the surface area of the sample containing 0.16 g MoO_3 per gram ZrO_2 reduces by two-fold, but the SA of pure ZrO_2 reduces by ten-fold. It is obvious that the presence of MoO_3 can improve the thermostability of the texture of ZrO_2 .

3.1.2. The results of XRD

The results of XRD show that there is a close relationship between the phase of ZrO_2 in a sample and its MoO_3 content. From figure 1, it can be seen that the ZrO_2 obtained by calcining pure $\text{Zr}(\text{OH})_4$ at 450°C for 4 h is a mixture of monoclinic (m) and tetragonal (t) phases; however, the fraction of ZrO_2 (t) in $\text{MoO}_3/\text{ZrO}_2$ with only a low content of MoO_3 increases obviously. As the content of MoO_3 is high enough, all ZrO_2 in $\text{MoO}_3/\text{ZrO}_2$ is tetragonal, and its XRD peaks become broader, which indicates that the ZrO_2 crystallite size gets smaller. As more MoO_3 is loaded, ZrO_2 is present as an amorphous phase.

After being calcined at 550°C, nearly all of $\text{Zr}(\text{OH})_4$ changes into monoclinic ZrO_2 . However, ZrO_2 obtained from $\text{Zr}(\text{OH})_4$ with sufficient Mo(VI) still appears as tetragonal ZrO_2 , even if calcined at 750°C (see figure 2). Obviously, Mo(VI) supported on $\text{Zr}(\text{OH})_4$ opposes the crystallization of ZrO_2 and the tetragonal to monoclinic transition.

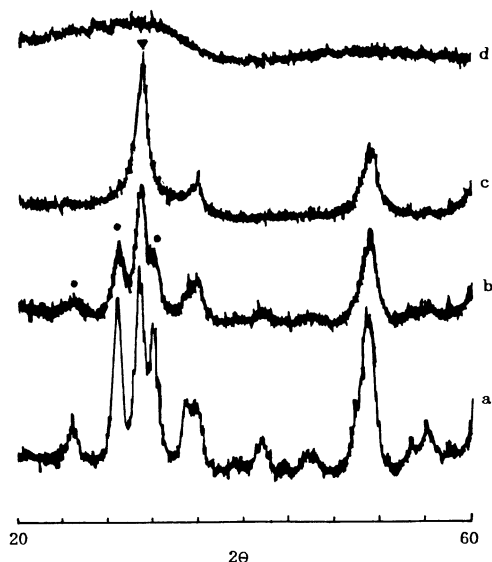


Figure 1. XRD patterns of $\text{MoO}_3/\text{ZrO}_2$ calcined at 450°C. MoO_3 content: (a) 0 (pure ZrO_2); (b) 0.03 g $\text{MoO}_3/\text{g ZrO}_2$; 0.16 g $\text{MoO}_3/\text{g ZrO}_2$; (d) 0.42 g $\text{MoO}_3/\text{g ZrO}_2$. (▼) Tetragonal ZrO_2 ; (●) monoclinic ZrO_2 .

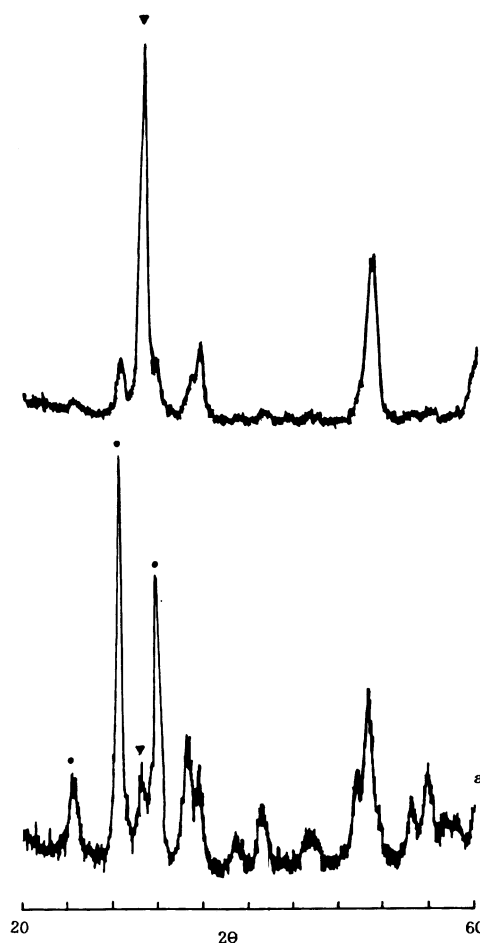


Figure 2. XRD patterns of some samples. (a) ZrO_2 calcined at 550°C; (b) $\text{MoO}_3/\text{ZrO}_2$ with 0.16 g $\text{MoO}_3/\text{g ZrO}_2$, calcined at 750°C.

3.1.3. DTA determination

The results in figure 3 show that the crystallization temperature for ZrO_2 from pure $\text{Zr}(\text{OH})_4$ is 452°C. However, for $\text{Zr}(\text{OH})_4$ with Mo(IV) (corresponding to 0.5 g $\text{MoO}_3/\text{g ZrO}_2$), the crystallization temperature of ZrO_2 increases by about 150°C, which means that the supported MoO_3 delays the crystallization process of ZrO_2 .

3.1.4. Results of Raman spectra

Raman spectra results for the phase of the support are corresponding to the XRD results. In addition, the results show that MoO_3 in $\text{MoO}_3/\text{ZrO}_2$ is dispersed on ZrO_2 as a monolayer. In the Raman spectra, a broad band at $\sim 950 \text{ cm}^{-1}$ is observed, which is assigned to a two-dimensional polymeric molybdate [13,14], and an additional broad band at $\sim 814 \text{ cm}^{-1}$ attributed to a Mo–O–Zr surface species appears [15]. Only when MoO_3 loading is above a certain level and the calcination temperature is over 500°C, a group of sharp peaks of bulk $\text{Zr}_2(\text{MoO}_4)_2$ at 750, 946, 1002 cm^{-1} appear (see figure 4). In this case, bulk $\text{Zr}_2(\text{MoO}_4)_2$ is also identified by XRD.

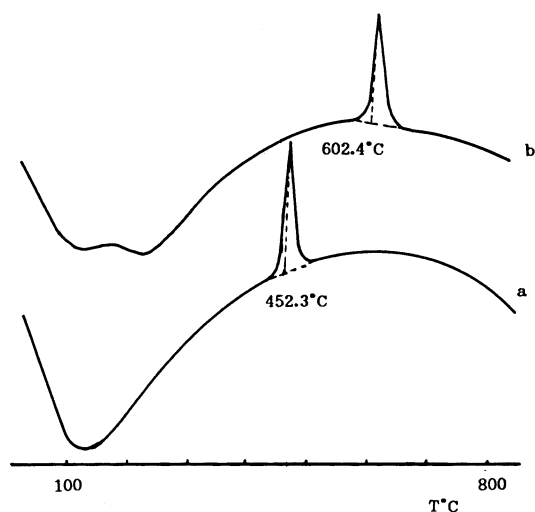


Figure 3. DTA results of Zr(OH)_4 and Zr(OH)_4 with $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}$. (a) Zr(OH)_4 ; (b) $(\text{NH}_4)_6\text{Mo}_7\text{O}_{24}/\text{Zr(OH)}_4$ (corresponding to 0.5 g $\text{MoO}_3/\text{g ZrO}_2$).

It is noteworthy that the surface area of the sample decreases rapidly as long as bulk $\text{Zr}_2(\text{MoO}_4)_2$ forms.

3.2. WO_3/ZrO_2 system

WO_3/ZrO_2 samples were prepared by impregnating Zr(OH)_4 (heated at 10°C) or ZrO_2 (calcined at 500 and 800°C respectively) with a solution of ammonium metatungstate, then calcining at 500 and 800°C respectively. Their specific surface areas are shown in table 2. The results show:

(1) The surface areas of support ZrO_2 obtained by heating pure Zr(OH)_4 at 500 and 800°C are 66 and $10 \text{ m}^2/\text{g}$ respectively. After supporting WO_3 , their SA decrease gradually with an increase in WO_3 content, which is in agreement with the general rule of the change in SA of most supported catalysts (table 2, columns B and E).

(2) WO_3/ZrO_2 samples obtained by impregnating Zr(OH)_4 are similar to $\text{MoO}_3/\text{ZrO}_2$ in the change of their SA with the content of the active component. The

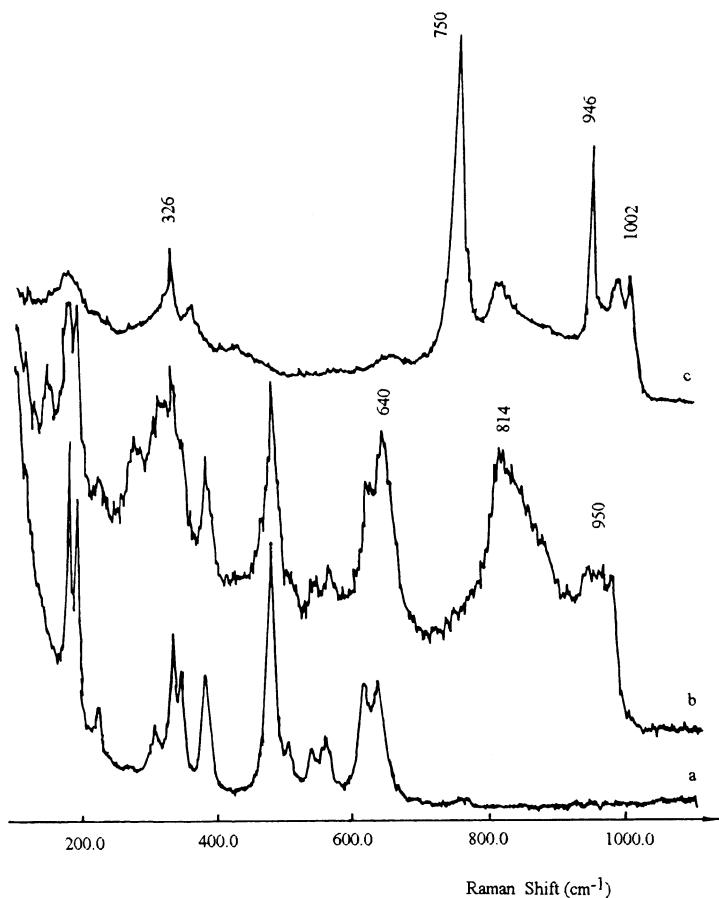


Figure 4. Raman spectra of $\text{MoO}_3/\text{ZrO}_2$. (a) ZrO_2 calcined at 550°C ; (b) $\text{MoO}_3/\text{ZrO}_2$ with 0.09 g $\text{MoO}_3/\text{g ZrO}_2$, calcined at 550°C ; (c) $\text{MoO}_3/\text{ZrO}_2$ with 0.42 g $\text{MoO}_3/\text{g ZrO}_2$, calcined at 550°C .

Table 2
The surface areas of WO₃/ZrO₂^a

WO ₃ content (g/g ZrO ₂)	SA (m ² /g)				
	calcined at 500°C		calcined at 800°C		
	A	B	C	D	E
0	66	66	10	10	10
0.05	76	66	44	52	< 10
0.15	175	64	73	50	< 10
0.20	185	63	60	48	< 10
0.30	225	60	57	46	< 10
0.40	227	57	50	42	< 10

^a A, C: Zr(OH)₄ was used as support; B, D: the support was calcined at 500°C.

S_{\max} of the samples calcined at 500°C is 3–4 times the SA of pure ZrO₂, and the S_{\max} of the samples calcined at 800°C is 7 times the SA of pure ZrO₂ (table 2, columns A and C).

(3) If the support is calcined at a lower temperature (such as 500°C), and then impregnated and calcined again at a higher temperature (such as 800°C), the surface areas of the resultant samples are much larger than those of the samples whose support has been calcined at 800°C (see table 2, columns D and E).

The above results show that the active component WO₃ can stabilize the texture for both Zr(OH)₄ and crystallized ZrO₂.

XRD results show that after being calcined at 800°C all of pure Zr(OH)₄ turns into monoclinic ZrO₂, whereas if impregnating Zr(OH)₄ with enough WO₃ before calcining at 800°C, the ZrO₂ in resultant WO₃/ZrO₂ is still present in tetragonal phase. The situation is quite similar to that of the MoO₃/ZrO₂ system.

In WO₃/ZrO₂ samples, WO₃ is present in a dispersion phase, which is manifested by a rise of a typical broad band at ~996 cm⁻¹ in their Raman spectra [16]. If WO₃ content exceeds a certain value, two narrow bands appear at 720 and 808 cm⁻¹ attributed to crystalline WO₃ [16]; however, the broad band at ~996 cm⁻¹ of the dispersion phase still exists, and its absolute intensity does not change yet (see figure 5). It has been found that the surface area of the sample is maximum when its WO₃ content corresponds to its utmost dispersion capacity on ZrO₂. For WO₃/ZrO₂, the utmost dispersion capacity is close to the geometric monolayer capacity, namely 0.19 g WO₃/100 m² support. The authors reported about this in detail in ref. [17].

3.3. CuO/ZrO₂ system

The surface area of CuO/ZrO₂ obtained by impregnating Zr(OH)₄ with a solution of Cu(NO₃)₂ and then calcining at 500°C is also larger than that of pure ZrO₂ obtained by calcining pure Zr(OH)₄ at the same temperature, as shown in table 3. It is obvious that the sup-

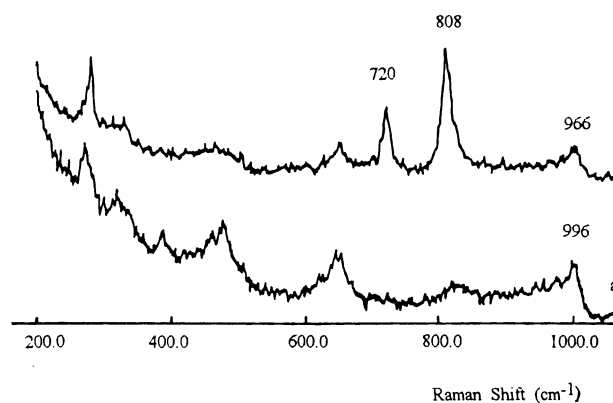


Figure 5. Raman spectra of WO₃/ZrO₂. (a) WO₃/ZrO₂ with 0.15 g WO₃/ZrO₂, calcined at 800°C; (b) WO₃/ZrO₂ with 0.20 g WO₃/ZrO₂, calcined at 800°C.

ported CuO can also stabilize the texture of ZrO₂. The XRD results show that CuO can also delay the crystallization of amorphous ZrO₂ and opposes the t → m transition of ZrO₂. The latter fact was reported by Shimikawabe et al. [18]. In figure 6, one can see that ZrO₂ in the samples with more CuO exists in amorphous state, while in those with less CuO, ZrO₂ is in tetragonal phase, although both of them are calcined at 500°C.

For identifying the state of CuO in CuO/ZrO₂, the XPS peak intensity ratios $I_{\text{Cu}2p}/I_{\text{Zr}3d}$ as a function of CuO content are determined, as shown in figure 7.

For CuO contents below 0.12 g/g ZrO₂, the slope of the $I_{\text{Cu}2p}/I_{\text{Zr}3d}$ versus CuO content curve is larger, which indicates all or a great majority of CuO exists on the surface of CuO/ZrO₂. When CuO content is beyond the above value, the slope decreases, which means the additional CuO occurs as a crystalline state or penetrates into the substrate. Since the amount of crystalline CuO detected by XRD is quite low, the later possibility cannot be excluded.

Comparing figure 7 with table 3, we find that the surface area of CuO/ZrO₂ increases gradually and approaches a maximum as the concentration of CuO on the surface increases, and the CuO content of the sample with S_{\max} is close to that at the turning point in the XPS $I_{\text{Cu}2p}/I_{\text{Zr}3d}$ curve. Obviously, it is the CuO dispersed on the surface of ZrO₂ that relaxes the loss of the surface area during calcination.

Table 3
The surface areas of CuO/ZrO₂

CuO content (g/g ZrO ₂)	Surface area (m ² /g ZrO ₂)
0	58
0.04	76
0.06	139
0.09	147
0.11	137
0.14	115

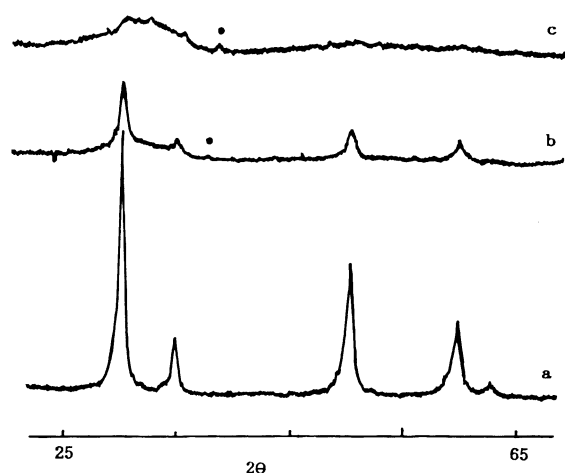


Figure 6. XRD patterns of CuO/ZrO_2 . CuO content: (a) 0.04 g $\text{CuO}/\text{g ZrO}_2$; (b) 0.11 g $\text{CuO}/\text{g ZrO}_2$; (c) 0.22 g $\text{CuO}/\text{g ZrO}_2$; (●) Crystalline CuO .

It is also noteworthy that the loading of CuO at the turning point of $I_{\text{Cu}2\text{p}}/I_{\text{Zr}3\text{d}}$ versus CuO content is only about half of its geometrical monolayer capacity on ZrO_2 , which indicates that CuO can only form a sub-monolayer covering on ZrO_2 . This is similar to the case of CuO on $\gamma\text{-Al}_2\text{O}_3$ [19].

The DTA measurements for these samples show that the crystallization temperatures of ZrO_2 in the samples shift up to 527°C (for CuO content of 0.06 g $\text{CuO}/\text{g ZrO}_2$) and 607°C (for CuO content of 0.25 g $\text{CuO}/\text{g ZrO}_2$), which indicates the dispersed CuO has a strong inhibition effect on the crystallization of ZrO_2 .

3.4. $\text{SO}_4^{2-}/\text{ZrO}_2$ system

Surface areas of the samples obtained by impregnating $\text{Zr}(\text{OH})_4$ with $(\text{NH}_4)_2\text{SO}_4$ solution and then calcining are also larger than that of pure ZrO_2 calcined at a same temperature, as shown in table 4. Obviously, the surface area of ZrO_2 can also be raised by supporting

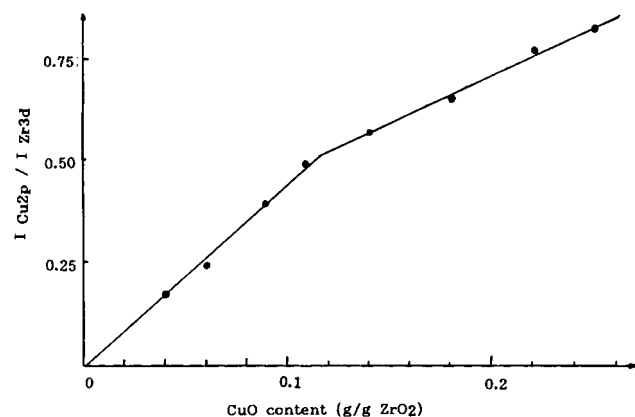


Figure 7. XPS $I_{\text{Cu}2\text{p}}/I_{\text{Zr}3\text{d}}$ versus CuO content of CuO/ZrO_2 .

Table 4
The surface areas of $\text{SO}_4^{2-}/\text{ZrO}_2$

SO_4^{2-} content (g/g ZrO_2)	SA ($\text{m}^2/\text{g ZrO}_2$)	
	calcined at 500°C	calcined at 800°C
0	56	27
0.06	125	60
0.08	146	83
0.11	150	91
0.14	156	103
0.17	125	96
0.20	112	80

SO_4^{2-} on it. XRD results show that the supported SO_4^{2-} can also restrain the crystallization of amorphous ZrO_2 and its $t \rightarrow m$ transition.

$I_{\text{S}2\text{s}}/I_{\text{Zr}3\text{d}}$ as a function of the content of SO_4^{2-} is shown in figure 8, from which we can see:

(1) The SO_4^{2-} in the sample with a low loading appears on the surface. As SO_4^{2-} content exceeds a certain value, the surface concentration of SO_4^{2-} does not change anymore, which means that the surplus SO_4^{2-} may have escaped as SO_3 during calcination.

(2) For the samples calcined at 500°C , the turning point of the $I_{\text{S}2\text{s}}/I_{\text{Zr}3\text{d}}$ versus SO_4^{2-} content curve corresponds to a SO_4^{2-} content of 0.11 g $\text{SO}_4^{2-}/\text{g ZrO}_2$, and the corresponding SA is $150 \text{ m}^2/\text{g ZrO}_2$. If the samples are treated at 650°C , the turning point corresponds to a SO_4^{2-} content of 0.07 g $\text{SO}_4^{2-}/\text{g ZrO}_2$, and its SA is about $80 \text{ m}^2/\text{g ZrO}_2$. Both are in good agreement with the utmost monolayer capacity estimated by assuming that SO_3 forms a close-packed layer [2–4], i.e., 0.08 g $\text{SO}_4^{2-}/100 \text{ m}^2 \text{ ZrO}_2$. However, we have also noticed that the SO_4^{2-} content in the sample with S_{max} is a little higher than its utmost monolayer capacity. The reason for the occurrence remains to be studied.

3.5. The other systems

The surface areas of all the samples prepared by impregnating $\text{Zr}(\text{OH})_4$ with solutions of $\text{Ni}(\text{NO}_3)_2$, $\text{Fe}(\text{NO}_3)_3$ and FeSO_4 and then calcining at 500°C are

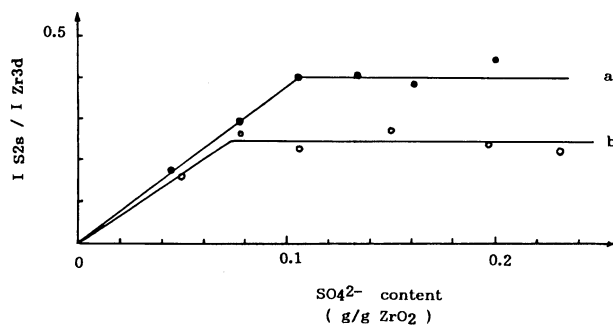


Figure 8. XPS $I_{\text{S}2\text{s}}/I_{\text{Zr}3\text{d}}$ versus SO_4^{2-} content of $\text{SO}_4^{2-}/\text{ZrO}_2$. Calcination temperature: (a) 500°C ; (b) 650°C .

also larger than pure ZrO₂ calcined at the same temperature. A part of the measurements and their corresponding contents of the active components are listed in table 5.

The XRD results show that in NiO/ZrO₂ there is little crystalline NiO, whereas in the other samples no XRD peak of the active components can be detected, which means that all or most part of these active components may occur as dispersion states. In addition, ZrO₂ in these samples is all present in tetragonal modification. These results suggest the universality of the above-mentioned phenomenon.

4. Discussion

It can be seen from the above-mentioned facts that if a layer of active component is covered on colloidal particles of Zr(OH)₄ before calcination, the resultant ZrO₂-supported catalysts often have much larger surface areas. The results of the above-listed seven catalysts, without exception, manifest this effect. Using this method, one can increase the surface areas of many ZrO₂-supported catalysts by several times and make them have a favorable comparison with those of the catalysts prepared from some classical supports (such as γ -Al₂O₃, SiO₂).

For all these catalysts under study, the surface areas increase gradually and reach their maxima, then decrease slowly with an increase in the loadings. The active components in all these systems can be dispersed on the surface of ZrO₂, and for each system, the S_{\max} occurs when the content of the active component is at its utmost dispersion capacity. Only in SO₄²⁻/ZrO₂ there appears a bit of discrepancy.

In table 6 the MoO₃ contents of MoO₃/ZrO₂ with S_{\max} are listed and compared with those of their theoretical monolayer capacities estimated from their real SA according to the close-packed monolayer model [2,20]. Obviously, they are in good agreement.

In addition, it can be seen that the effectiveness of these components in increasing the surface area is different. MoO₃, WO₃, SO₃ and FeSO₄ can form a quite complete monolayer on ZrO₂, while the dispersion capacities of CuO and NiO on ZrO₂ are only about a half of their theoretical values, which means CuO and NiO can only form a sub-monolayer on ZrO₂ [19,21]. The above

Table 6
The maximum specific surfaces of MoO₃/ZrO₂ and their corresponding MoO₃ contents

Calcination temp. (°C)	S_{\max} (m ² /g ZrO ₂)	MoO ₃ content (g/g ZrO ₂)	Close-packed monolayer capacity (MoO ₃ /g ZrO ₂)
450	310	0.31	0.37
550	225	0.27	0.27
600	195	0.24	0.23
750	100	0.12	0.12

results show that MoO₃, WO₃, SO₃ and FeSO₄ are more effective in increasing the surface area. The reason is that the more completely the surfaces of colloidal grains of ZrO₂ are covered, the more effectively these grains are separated from each other, and the more the surface diffusion of ZrO₂ is suppressed. In this case, the structure of ZrO₂ grain becomes more stable, thus the surface area of ZrO₂-supported catalyst can be maintained better during heat treatment.

However, when the content of an active component exceeds its utmost dispersion capacity, the surplus will appear as crystalline phase to block up the pores of the support (such as in WO₃/ZrO₂) or form a new compound with ZrO₂ at a relatively high temperature (such as Zr(MoO₄)₂ in MoO₃/ZrO₂). In these cases, the surface area of a sample will decrease.

The effects of the active components put onto the surface of ZrO₂ in advance can be summed up as follows:

(1) To raise the crystalline temperature of amorphous ZrO₂ obtained from dehydration of Zr(OH)₄.

(2) To make ZrO₂ as support preserve in the metastable tetragonal phase at higher calcination temperature instead of turning into the monoclinic phase, and the size of crystalline ZrO₂ grains smaller.

(3) An active component covering on the ZrO₂ calcined and crystallized at a relatively low temperature can still suppress ZrO₂ grains growing up further at higher temperature, and as a result, the trend of a drastic decrease in the surface area of the catalyst during calcination would be relaxed.

Turning amorphous ZrO₂ into crystalline ZrO₂, turning metastable tetragonal into stable monoclinic modification and inter-crystalline sintering among fine grains of ZrO₂ all depend on the stability of the structure of ZrO₂ grains [1,9]. It is by stabilizing the structure of the grains that the active components give rise to the above-mentioned effects and lead to the surface area stabilization observed.

In studies on superplastic structural ceramics it was found that Y³⁺ can stabilize tetragonal ZrO₂ [9]. In addition, it was also pointed out that additive divalent or trivalent cations are enriched at the grain-boundary, which segregate strongly the grain-boundary and lower the grain-boundary mobility and the grain-boundary energy. Obviously, the same principle is coming into play for both the ceramics and the catalyst systems men-

Table 5
The surface areas of some samples

Sample	Content of active component (g/g ZrO ₂)	SA (m ² /g ZrO ₂)
ZrO ₂	0	48
NiO/ZrO ₂	0.14	80
Fe ₂ O ₃ /ZrO ₂	0.10	87
FeSO ₄ /ZrO ₂	0.19	143

tioned above. Recently, Y^{3+} and La_2O_3 were also used for stabilizing tetragonal ZrO_2 in some catalyst systems [22].

It should be pointed out that since the chemical properties of $\text{Zr}(\text{OH})_4$ are more active than those of ZrO_2 , the probability of the surface or bulk reaction between $\text{Zr}(\text{OH})_4$ and active component cannot be ignored. Therefore, the state of the active component in the catalyst prepared from $\text{Zr}(\text{OH})_4$ might change to some extent. For example, it has been described above that in Raman spectra of $\text{MoO}_3/\text{ZrO}_2$ prepared from $\text{Zr}(\text{OH})_4$ a new characteristic broad band at about 812 cm^{-1} occurs, which is attributed to a Mo–O–Zr surface species, and as MoO_3 content exceeds its utmost dispersion capacity the crystalline $\text{Zr}(\text{MoO}_4)_2$ appears after calcination at 550°C . Whereas, for $\text{MoO}_3/\text{ZrO}_2$ prepared from crystallized ZrO_2 the Raman band at $\sim 812\text{ cm}^{-1}$ does not appear, and the surplus MoO_3 still exists as crystalline MoO_3 even if calcined at higher temperature [15]. Therefore, it can be expected that there might be some differences between a catalyst from ZrO_2 and that from $\text{Zr}(\text{OH})_4$ in their catalytic behavior. As the interaction between the support and an active component is strong, the difference would become more obvious. It is a typical example that $\text{MoO}_3/\text{ZrO}_2$, WO_3/ZrO_2 and $\text{SO}_4^{2-}/\text{ZrO}_2$ prepared from $\text{Zr}(\text{OH})_4$ possess superacidity but those prepared from ZrO_2 do not [6,7]. So using the method recommended in this paper to prepare a catalyst, one must pay attention to whether its properties in adsorption and catalysis change or not.

In some cases, we suggest a compromise proposal, namely, calcining $\text{Zr}(\text{OH})_4$ at a relatively low temperature to turn it into ZrO_2 with a quite high surface area, then impregnating it with the solution of an active component or its precursor and calcining it again at the high temperature required in a desired application. Since during the second calcination the active component can still suppress grain growth of ZrO_2 and the inter-grain sintering, one can obtain a catalyst whose specific surface is larger and whose change in surface properties is slight.

We find that the above-mentioned effects also exist in TiO_2 or Al_2O_3 -supported catalysts to some extent, which will be reported subsequently.

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References

- [1] P.D.L. Mercera, J.G. van Ommen, E.B.M. Doesburg, A.J. Burggraaf and J.R.H. Ross, *Appl. Catal.* 57 (1990) 127.
- [2] Y.C. Xie and Y.Q. Tang, *Adv. Catal.* 37 (1990) 1.
- [3] Y.C. Xie, L.L. Gui, Y.J. Liu, B.Y. Zhao, N.F. Yang, Y.F. Zhang, Q.L. Guo, L.Y. Duan, H.Z. Huang, X.H. Cai and Y.Q. Tang, in: *Proc. 8th Int. Congr. on Catalysis* (Verlag Chemie, Weinheim, 1984) 5, 147.
- [4] Y.C. Xie, L.L. Gui, Y.F. Zhang, B.Y. Zhao, N.F. Yang, Q.L. Guo, L.Y. Duan, H.Z. Huang, X.H. Cai and Y.Q. Tang, in: *Adsorption and Catalysis on Oxide Surface*, eds. M. Che and G.C. Bond (Elsevier, Amsterdam, 1985) p. 139.
- [5] B.Y. Zhao, H.Z. Liu, L.L. Gui and Y.Q. Tang, *J. Catal. (China)* 8 (1987) 413.
- [6] K. Arata and M. Hino, *Mater. Chem. Phys.* 26 (1990) 213.
- [7] K. Arata, *Adv. Catal.* 37 (1990) 165.
- [8] A. Cimino, D. Cordischi, S. De Rossi, G. Ferraris, D. Gozzoli, G. Minelli, M. Occhuzzi and M. Valigi, *J. Catal.* 127 (1991) 744.
- [9] I. Wei and X. Liang An, *J. Am. Ceram. Soc.* 73 (1990) 2585.
- [10] C. Xu, J. Tamaki, N. Miura and N. Yamazoe, *J. Mater. Sci. Lett.* 8 (1989) 1092.
- [11] C. Xu, J. Tamaki, N. Miura and N. Yamazoe, *Sensors and Actuators B* 3 (1991) 147.
- [12] Keshavaraja, B.S. Jayashri and A.V. Ramaswamy, *Sensors and Actuators B* 3 (1995) 75.
- [13] J. Medema, C. van Stam, V.H.J. de Beer, A.J.A. Konings and D.C. Koningsberger, *J. Catal.* 53 (1978) 386.
- [14] H. Knözinger and H. Jeziorowski, *J. Phys. Chem.* 82 (1978) 2002.
- [15] B.Y. Zhao, X.Y. Wang, H.R. Ma and Y.Q. Tang, *Mol. Catal. A* 108 (1996) 167.
- [16] S.S. Chan, I.E. Wachs, L.L. Murrell and N.C. Dispenziere, *J. Catal.* 92 (1985) 1.
- [17] B.Y. Zhao, X.P. Xu, J.M. Gao and Y.Q. Tang, *J. Raman Spectrosc.* 27 (1996) 549.
- [18] M. Shimokawabe, H. Asakawa and N. Takezawa, *Appl. Catal.* 59 (1990) 45.
- [19] B.Y. Zhao, Y.F. Zhang, L.Y. Duan, Y.C. Xie and Y.Q. Tang, *J. Catal. (China)* 39 (1982) 101.
- [20] Liu, Y.C. Xie, J. Ming, J. Liu and Y.Q. Tang, *J. Catal. (China)* 39 (1982) 262.
- [21] Zhang, Y.C. Xie, Y. Zhang, D.L. Zhang and Y.Q. Tang, *Sci. Sin. Ser. B (Chin. Ed.)* 8 (1986) 805.
- [22] P.D.L. Mercera, J.G. van Ommen, E.B.M. Doesburg, A.J. Burggraaf and J.R.H. Ross, *Appl. Catal.* 78 (1991) 79.